


Reinhold Environmental Ltd.



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Presentation***

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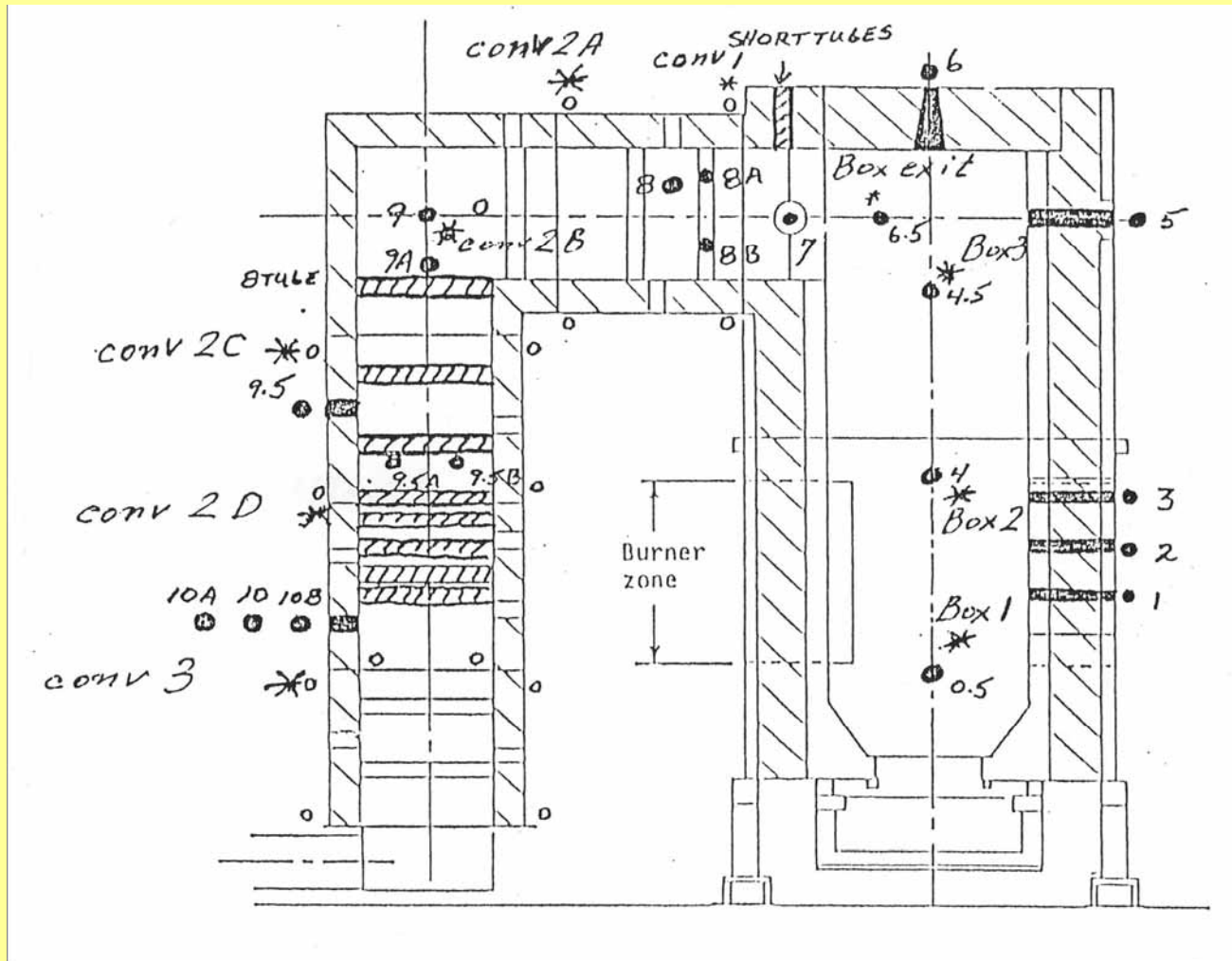
**Alternate Technology for
Enhanced SO_x/NO_x Capture
by Limestone-Urea Injection**

**By T. Steven Torbov
Aptech Engineering Services, Inc.
Sunnyvale, California**

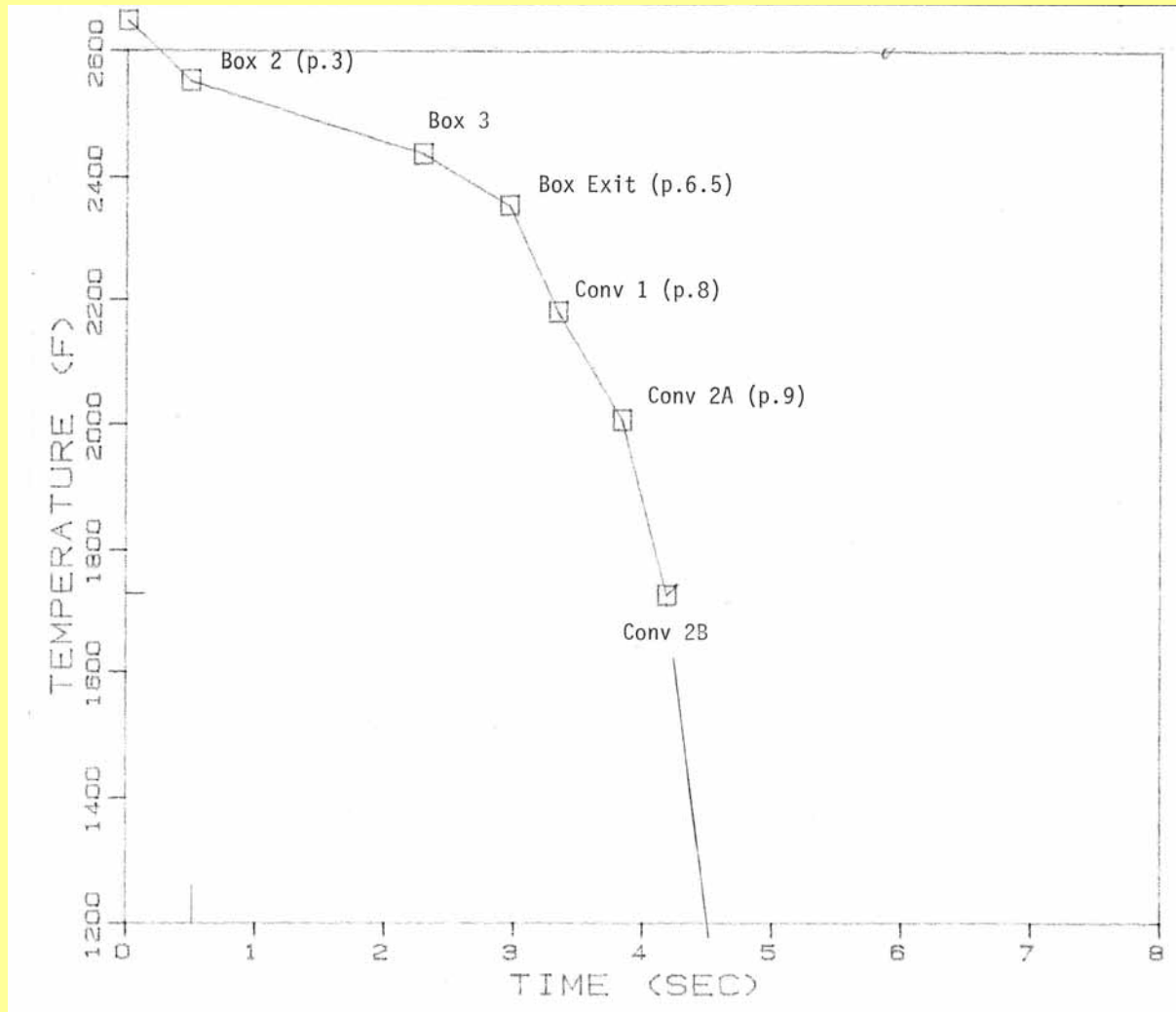
Limestone Sorbent Injection in a Pilot Scale Furnace

- **Limestone injection in a pilot scale furnace with capacity 1.3 MMBTU/hr**
- **Furnace operated on natural gas doped with H₂S (simulation of Illinois Coal #6)**
- **Sorbent – El Dorado dry limestone ground down to 40-50 microns**
- **Model the temperature-time profile for the full scale coal fired utility boilers U.S. design with capacity 200 MW to 500 MW**

Location of Ports and Wall Thermocouples



Temperature – Time Profile Dry Limestone P.3, P.5, P.8, P.9 No. 1, 3, 4, 5, 6, 7



Baseline Particle Temperatures

- Sorbent injection over the burner zone
- Temperatures at injection: 2500 to 2280°F (1400 to 1250°C)
- Radiation heat transfer dominates
- Time to achieve 2300°F (1245°C) particle temperatures:

11 Micron	0.9 MSEC
45 Micron	15 MSEC

Characteristic Time-Temperatures

- **Sorbent process times**
 - **Calcination: 0.2 to 0.3 seconds**
 - **Sulfation: 0.35 to 0.4 seconds**
 - **Total calcination and sulfation: 0.7 seconds**
- **Sorbent process temperatures**
 - **Calcination: 2200 to 1800°F**
 - **Sulfation: 2000 to 1750°F – limestone**
 - **Sulfation: 2000 to 1300°F - dolomite**

Dry Sorbent Baseline Results

N	Sorbent Injection		SO ₂ Reduction (%)	Ca/S Ratio	Ti-Tg (°F)	$\tau_i - \tau_g$ (sec)	SR	SO ₂ Input (ppm)
	Port Location	Direction						
1	3	Coflow	35.85	2.52	2535 – 2000	3.35	1.19	3975
3	5	Coflow	35.87	2.59	2400 – 2000	1.6	1.18	3875
4	8	Counter flow	34.21	2.40	~2400 – 2000	<0.5	1.21	3950
5	8	Cross flow	34.36	2.40	2190 – 2000	~0.5	1.21	3950
6	9	Counter flow	45.33	2.40	~2100 – 2000	<0.5	1.20	3975
7	9	Coflow	15.28	2.40	2000	--	1.20	3950



Sorbent Deactivation

- **Critical temperature – 1950 to 2000°F**
- **Time for particle deactivation – 1 to 15 MSEC**

Enhanced SO₂ Capture

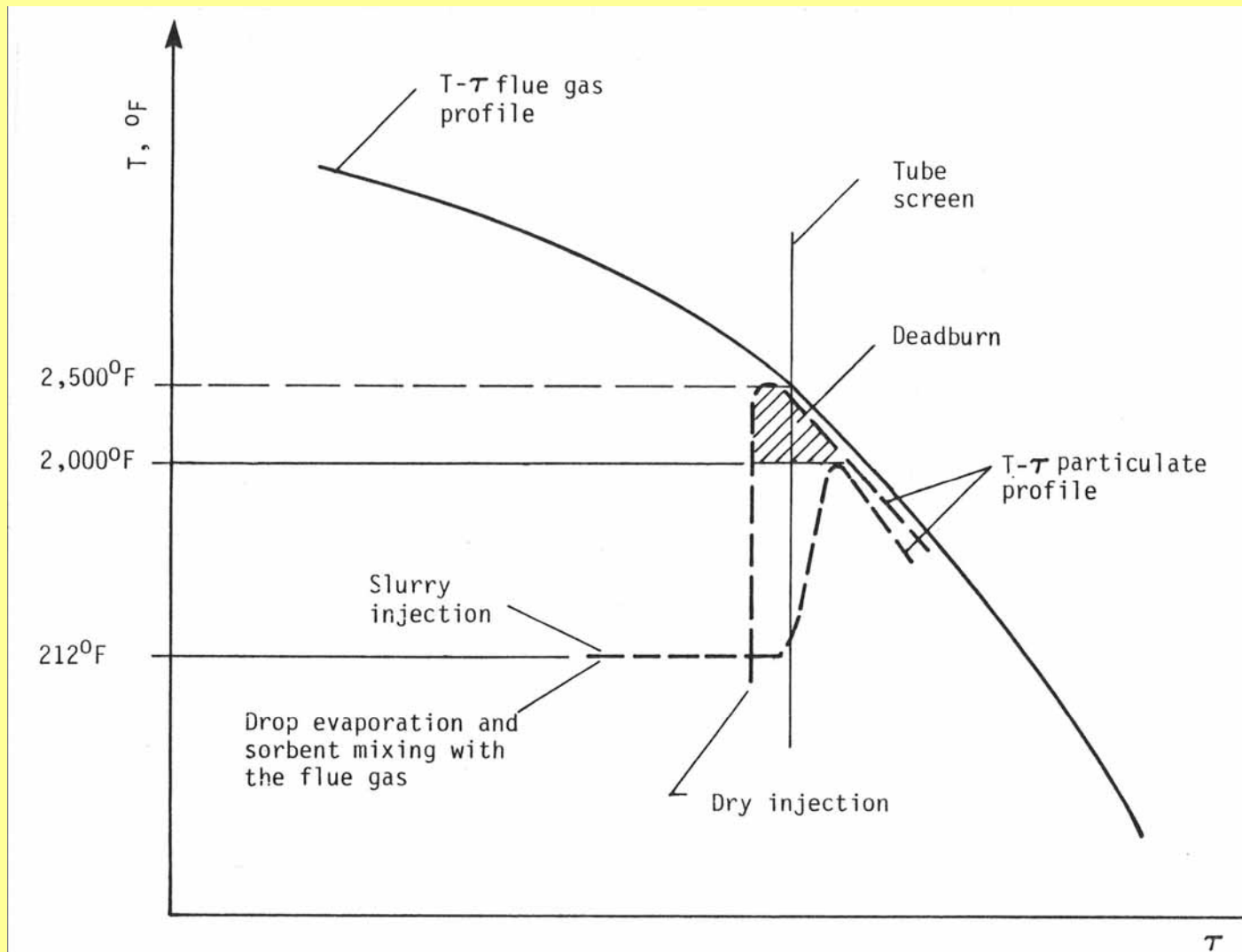
- **Inject water/limestone slurry (2:1) jet supported by air**
 - **Upper Furnace**
 - **Good penetration and distribution**
 - **Good mixing (~1 sec residence time)**
- **Suppress sorbent deactivation**
 - **Low particle temperatures during evaporation**
 - **Water drop evaporation time: 0.8 – 1 sec**
 - **Achieve desirable sorbent particulate temperature zone - 2000°F (behind the tube screen and first row superheater tubes)**



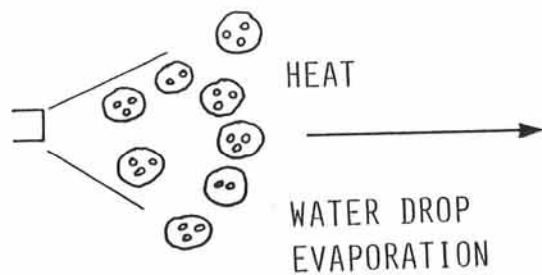
Slurry Injection Advantages

- **Suppress deadburning**
- **Enhanced mixing**
- **Desired temperature window hit in inaccessible areas**
- **Ash interaction avoided**
- **Opportunity to use water as an additional additive-carrying medium**

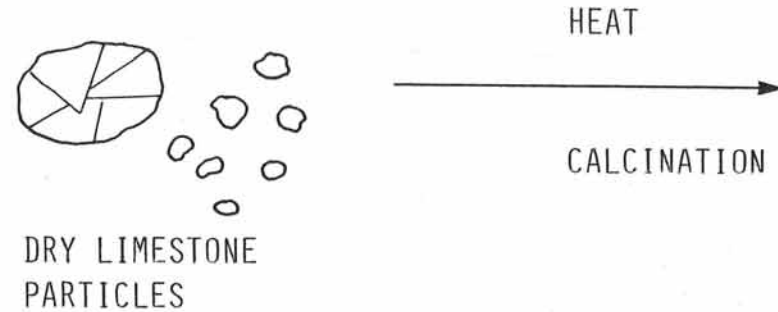
Sorbent Injection Process



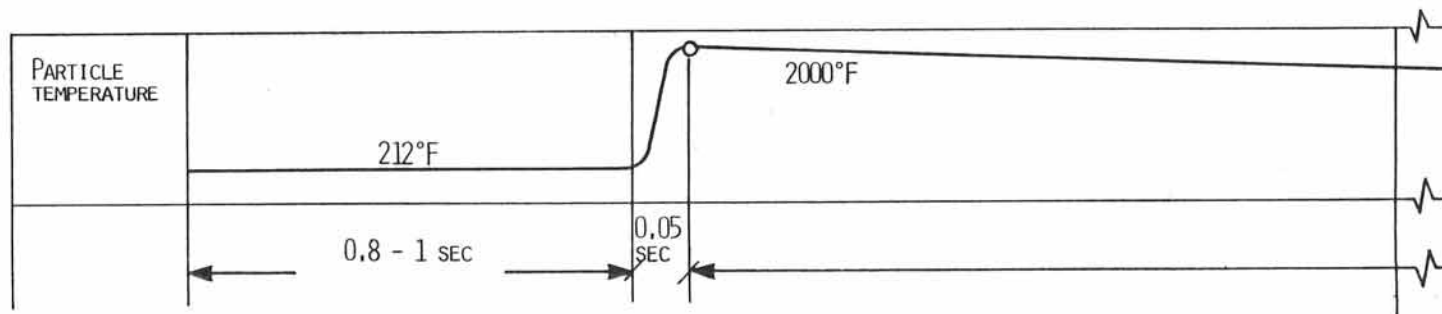
Enhanced SO₂ Capture



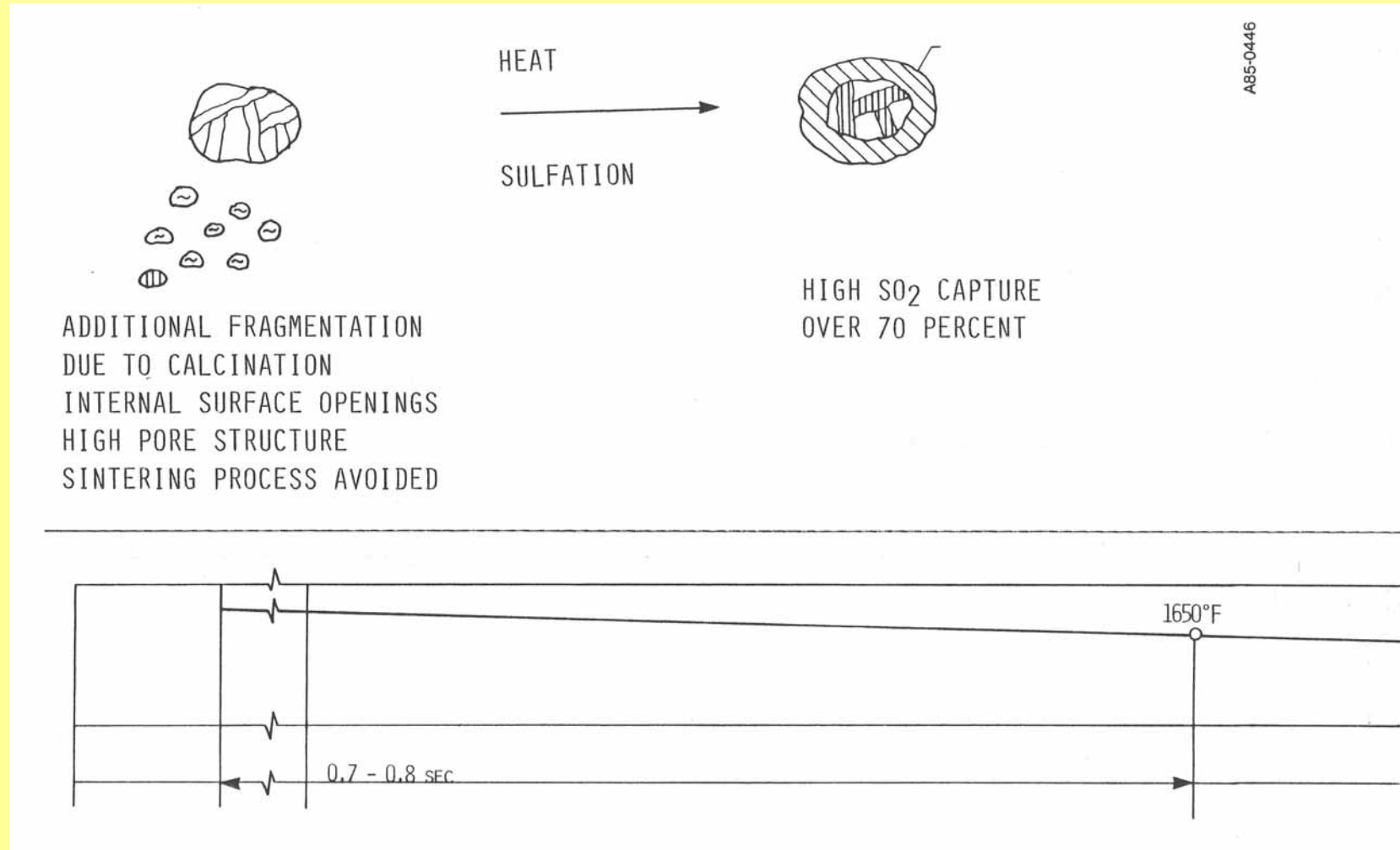
LIMESTONE-WATER SLURRY ATOMIZATION
GOOD MIXING WITH FLUE GAS FLOW



PARTICLE DISINTEGRATION DUE TO INCREASED
VAPOR PRESSURE IN THE PORE STRUCTURE



Enhanced SO₂ Capture



Time to Heat Up Water Drops to Reach Boiling Surface Temperature

Drop Diameter δ, μ	200	300	500	800	1000	1500
Time τ, SEC	3.24×10^{-3}	7.29×10^{-3}	2.03×10^{-2}	5.18×10^{-2}	8.1×10^{-2}	1.82×10^{-1}

Evaporation Time of Water Drops Injected in a Gas Flow

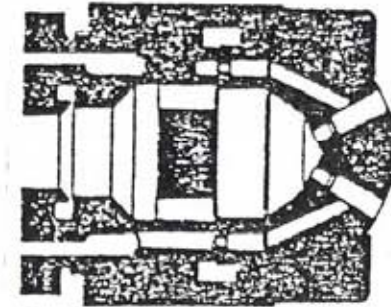
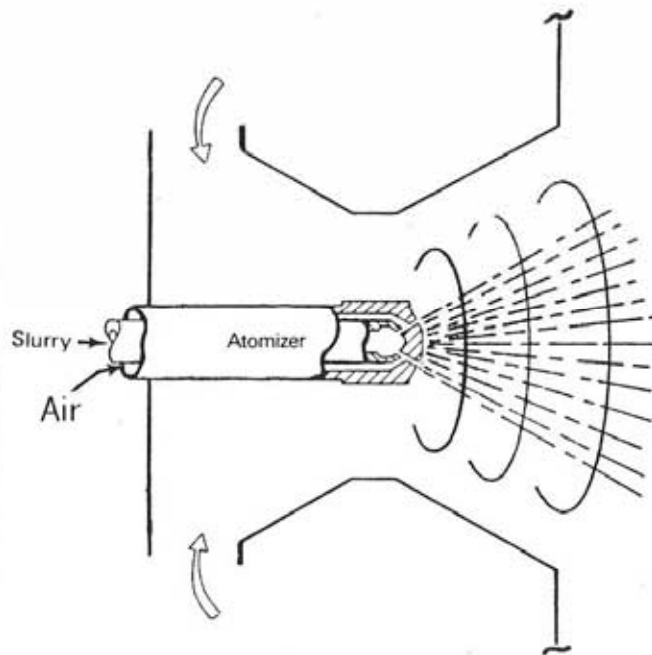
Drop Diameter δ, μ	200	300	500	800	1000	1500
Time τ, SEC	0.021	0.048	0.133	0.339	0.530	1.193

Gas Flow Temperature 2192°F (1200°C)

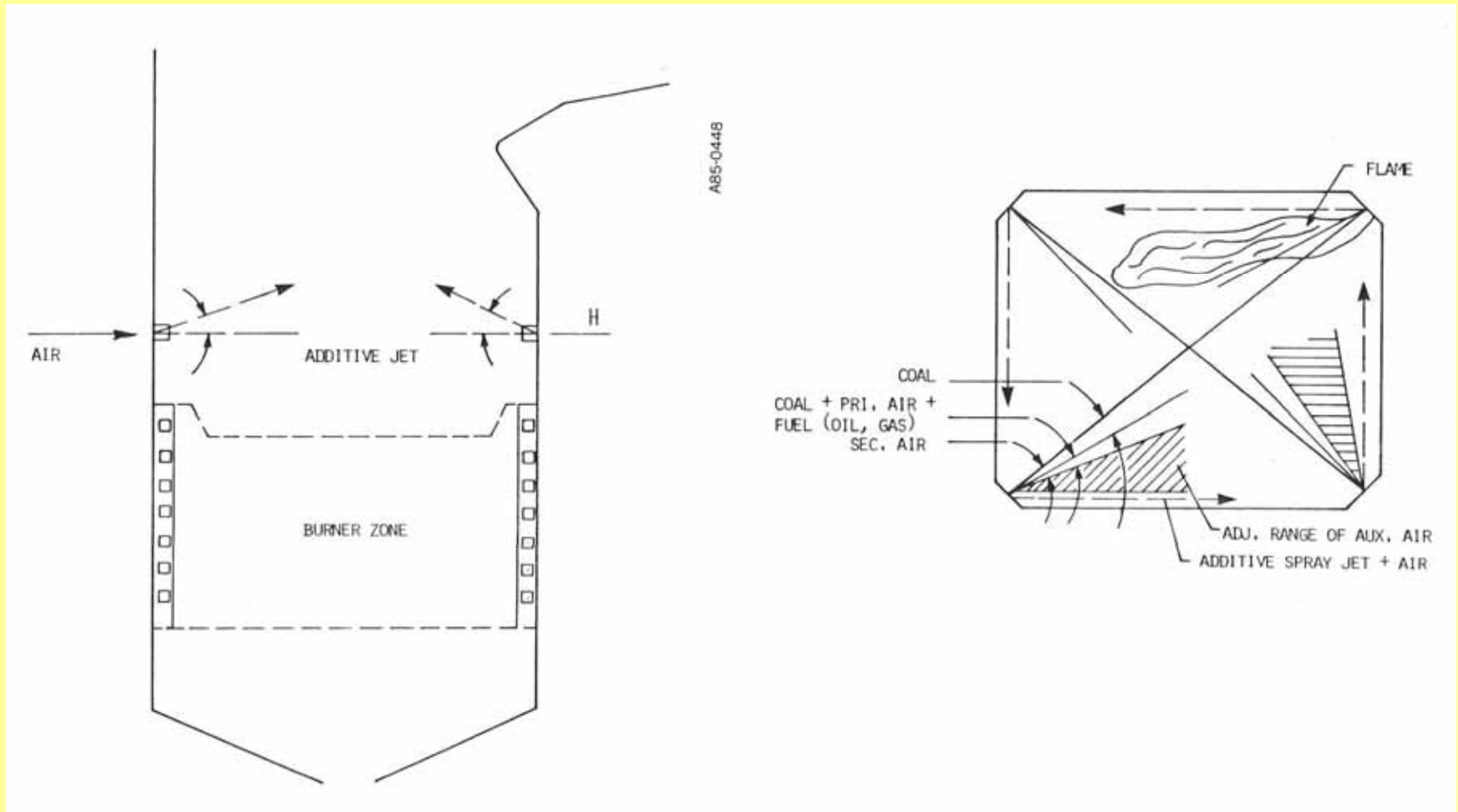
Slurry Atomization and Injection

FGR 5 to 10 Percent

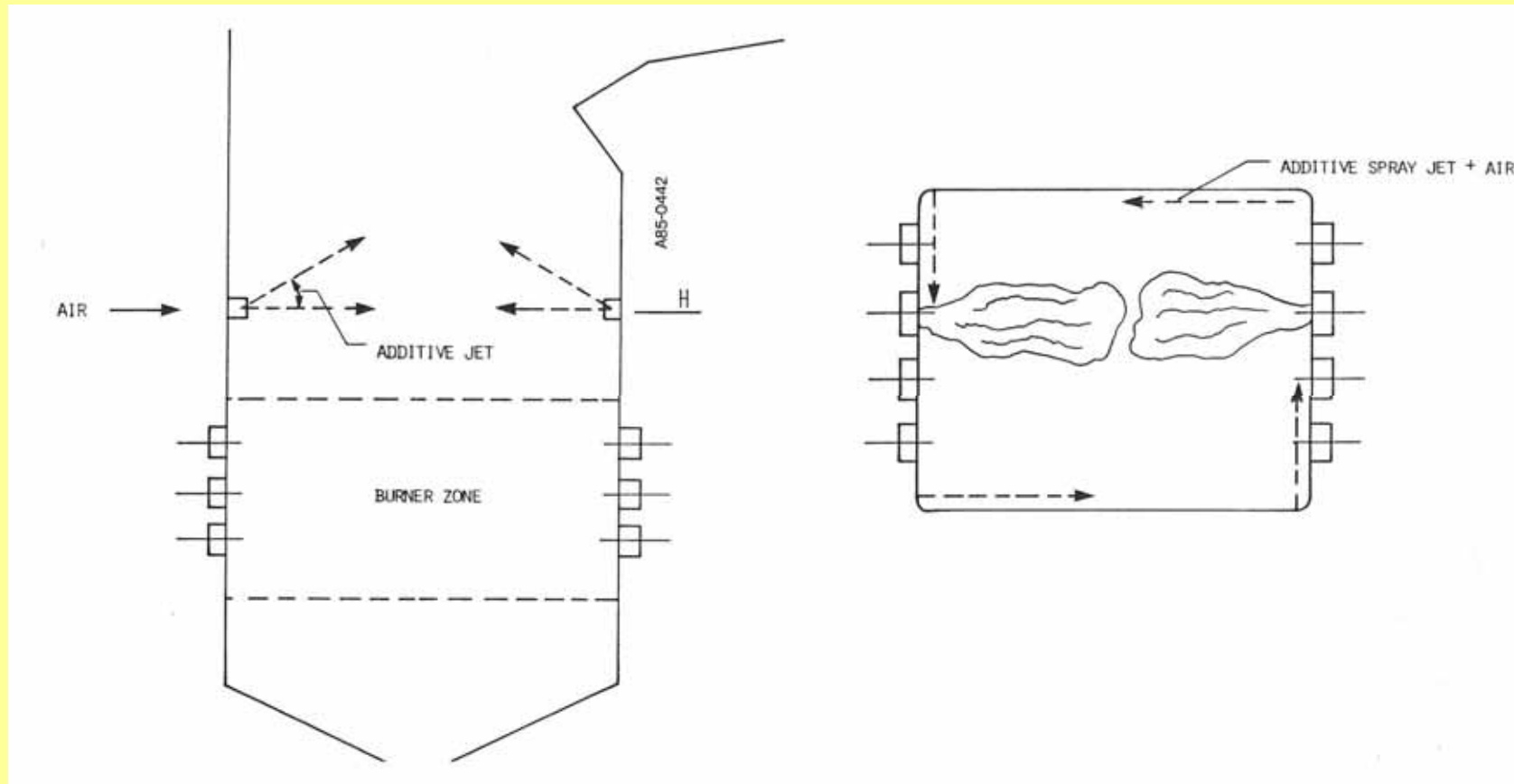
Compressed Air 45 to 60 psi
Slurry 30 psi



T-Fired Boiler



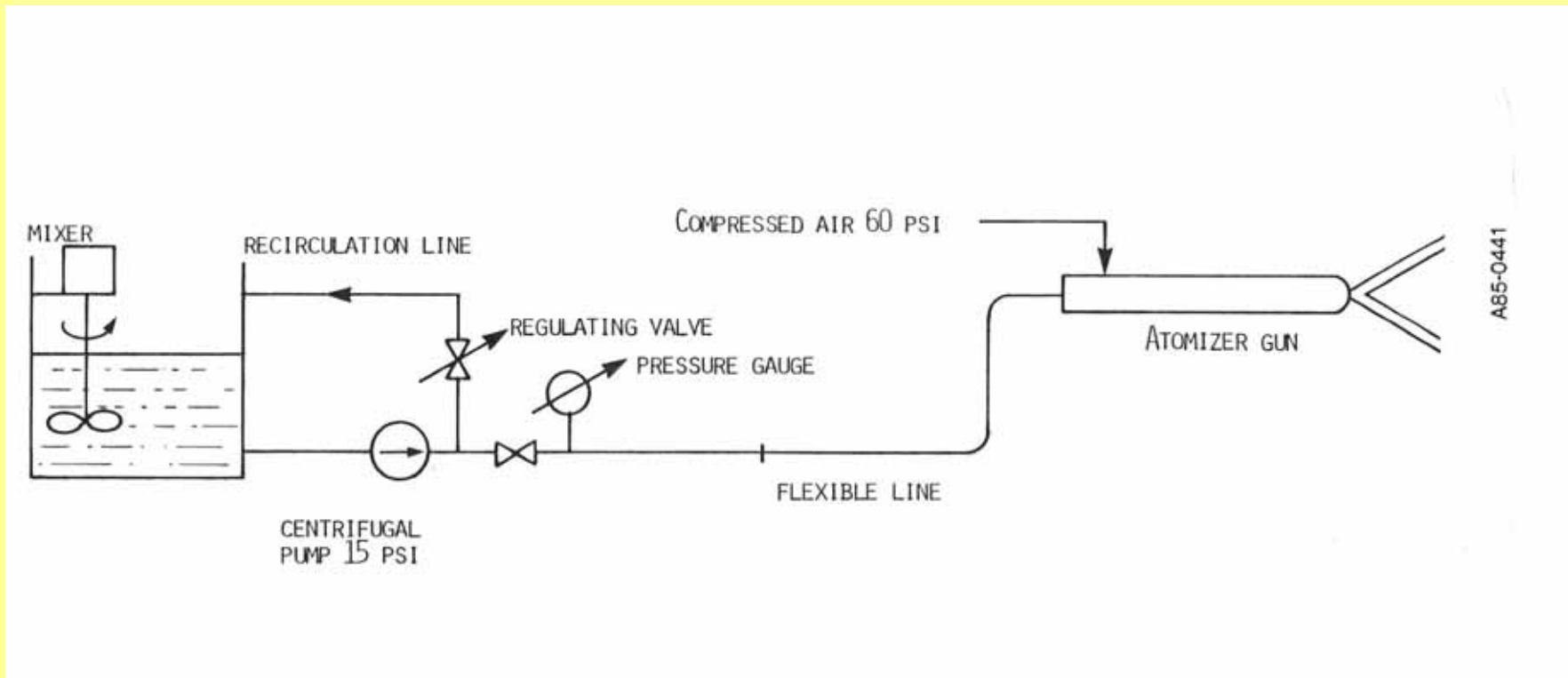
Wall-Fired Boiler



Preliminary Limestone – Water Slurry Tests

- Natural gas doped with H₂S (Illinois Coal #6 Simulation)
- 1.3 MBTU/hr T-fired furnace
- Sorbent: Fine El Dorado limestone
- Slurry: 1:2 ratio sorbent/water
- Injection: Different ports in the furnace – Y-jet atomizer
- Mixing problem with flue gas avoided

Limestone Slurry Experimental Equipment



Slurry Results

N	Slurry Sorbent Injection		SO ₂ Reduction (%)	Ca/S Ratio	Ti-Tg (°F)	$\tau_i - \tau_g$ (sec)	α	SO ₂ Input (ppm)
	Port Location	Direction						
1	5	Coflow	72.58	2.69	2160 – 1830	2.0	1.20	3875
2	5 Moved Injector 2" Ahead	Coflow	76.50	2.69	2160 – 1830	2.0	1.21	3875
3	5	Coflow	35.82	2.57	2380 – 1980	1.3	1.18	3975
4	5	Coflow	38.42	2.57	--	--	1.18	3975

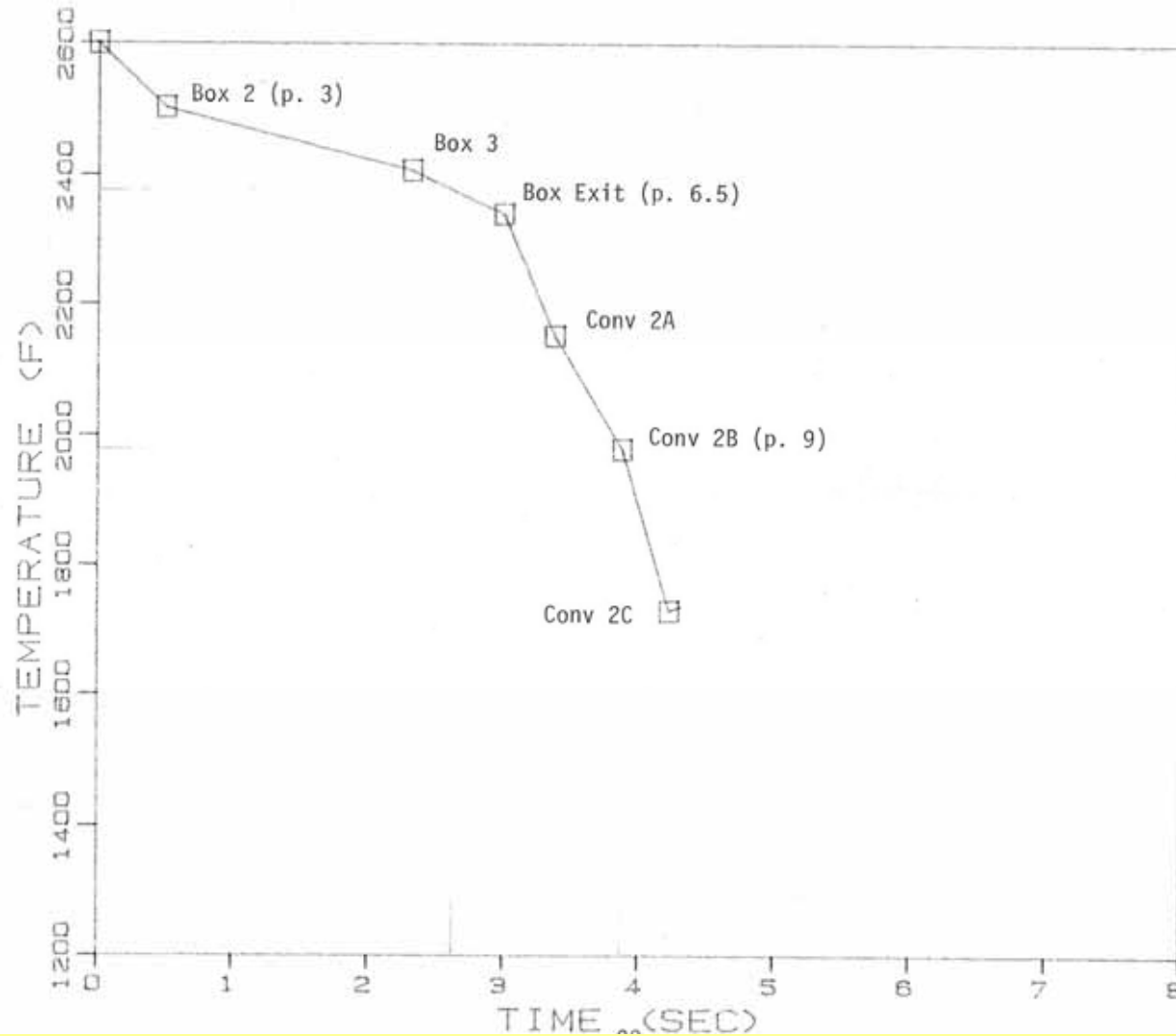
Natural gas doped with H₂S (simulation of Illinois Coal #6)

Sorbent: 1 & 2 – El Dorado limestone slurry 1:3

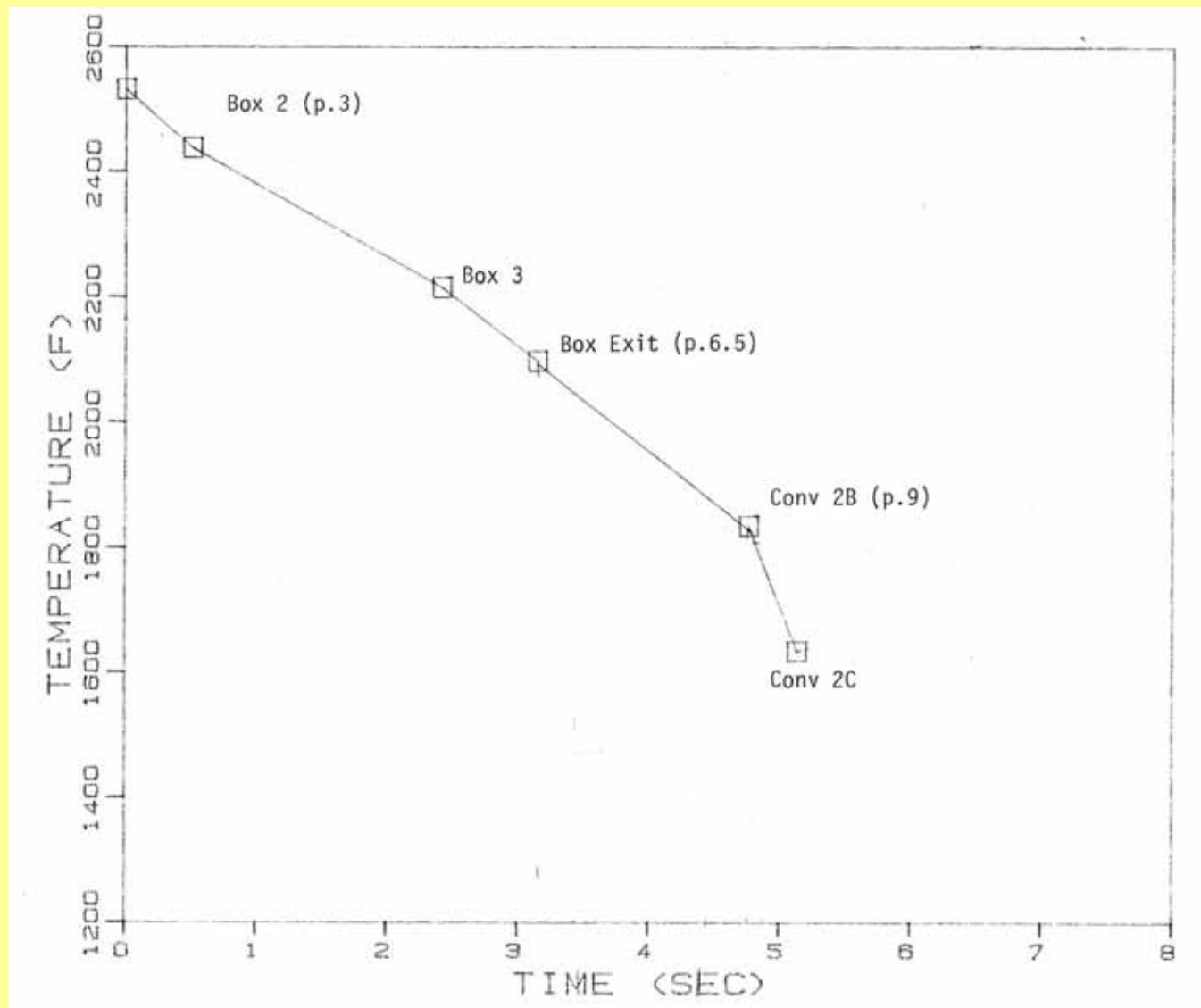
3 – El Dorado dry limestone

4 – El Dorado dry limestone P3, equivalent water P3 to 1:3

Baseline for 1, 2, and 3



Slurry 1:3, 5, Tests 1 and 2



Boiler Performance Impact

- **No impact on the steam parameters and SH/RH performance**
- **No impact on boiler capacity**
- **Insignificant boiler efficiency decrease because water injection**
- **No influence on combustion stability**
- **Primary SH/RH and economizer erosion evaluation**
- **FD and ID capacity and pressure evaluation**
- **ESP/Baghouse capacity and performance evaluation**

Boiler Parameters

■ Capacity

- 230 T/hr (507,000 lb/hr) steam

■ Pressure

- After superheater – 101 ATM (1485 psi)
- Boiler drum – 110 ATM (1620 psi)

■ Temperature

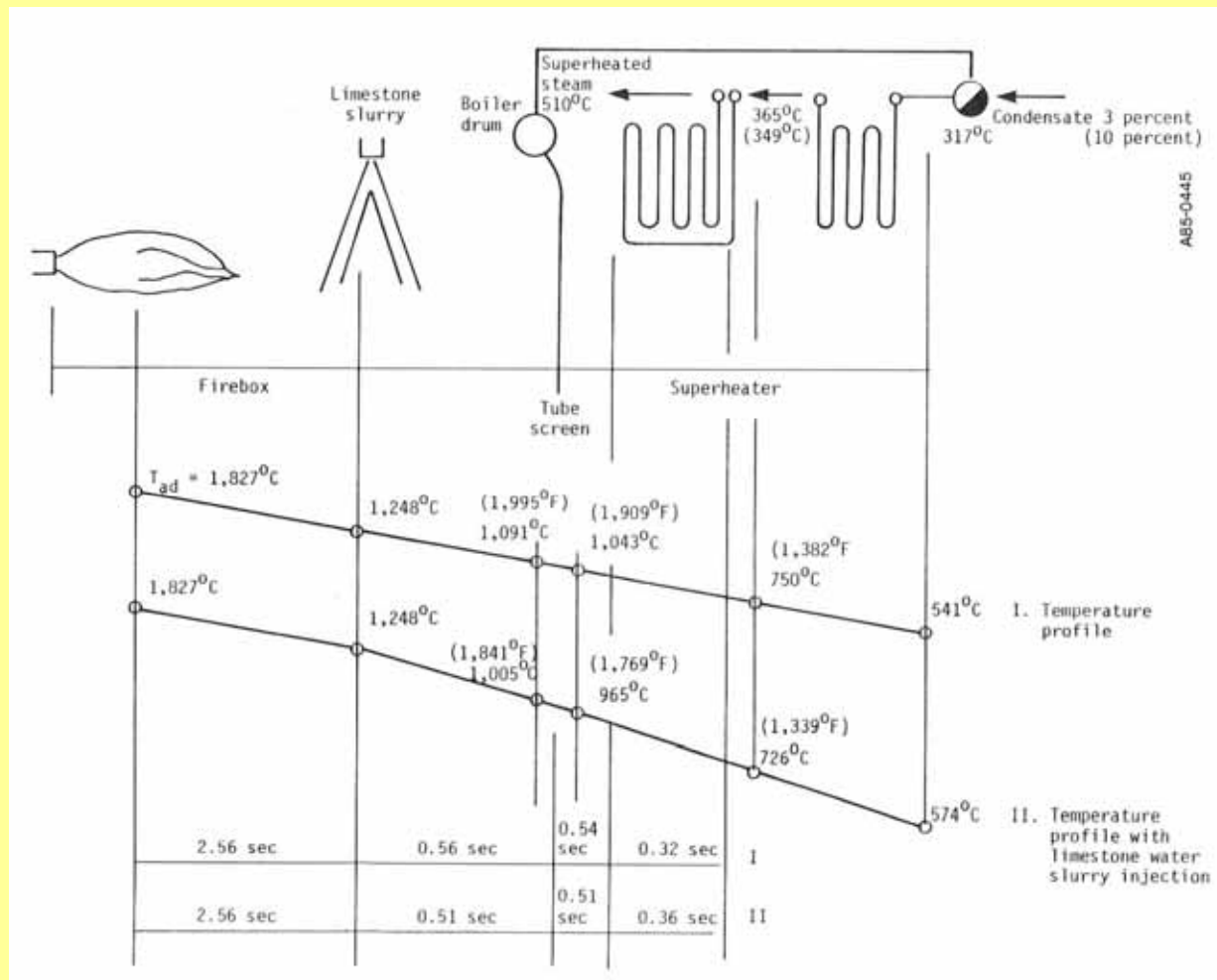
- Superheater steam – 510°C (950°F)
- Feeding water – 215°C (419°F)

Boiler Parameters – Cont.

■ Coal – Subbituminous Coal

- W – 11.0%
- A – 40.1%
- S – 3.8%
- C – 38.6%
- H – 2.6%
- N – 0.8%
- O – 3.1%
- Vol – 30.0%
- LHV – 3650 KCAL/KG (6570 BTU/lb)

Boiler Profiles with and without Slurry Injection



Flue Gas NO_x Control with Urea Injection

- Urea injection technology based on EPRI patent, now expired and is public domain
- In the small scale furnaces with good mixing of urea with the flue gas 80% NO_x reduction achieved
- In a real boiler not more than 40% NO_x reduction achieved because the mixing problem

Flue Gas NO_x Control with Urea Injection – Cont.

- APTECH system provides a good mixing of urea with main flue gas flow in the right temperature window
- Urea temperature window – 1500°F to 1900°F
- Ca based sorbent temperature window – 1600°F to 1850°F
- Expected NO_x reduction with APTECH system – up to 75%